PID tuning tackling design tradeoffs from an unified perspective

# Ramon Vilanova Dept. Telecomunications and Systems Engineering Universitat Autónoma de Barcelona, Barcelona

Workshop "Advanced Topics in PID Control System Design, Automatic Tuning and Applications" 21st IFAC World Congress, Germany July 12, 2020

# Motivation

- 2 Problem statement and generic solution
- 3 Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation
- 6 Concluding Remarks

# 1 Motivation

- 2 Problem statement and generic solution
- **3** Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 6 PID Tuning guidelines for Balanced Operation
- 6 Concluding Remarks

The universality and resilience of the PID is made explicit with the following sentences from a 2009's article at Machine Design<sup>†</sup>

- The main benefit of any PID loop is that a designer can "set it and forget it" while still maintaining a well-regulated system.
- PID control is so universal ... PID loops provide technicians and engineers with a customizable way to control a variety of conditions, from temperature to speed and everything in between.

if PID didn't already exist we would be forced to invent it, or factory automation would be very limited.

†Paul Avery Senior Product Training Engineer, Yaskawa Electric, America

Problem statement and generic solution Specific Tuning Rules Robustness and Performance evaluation PID Tuning guidelines for Balanced Operation Concluding Remarks

### A Survey on Industry Impact and Challenges Thereof

FEBRUARY 2017 « IEEE CONTROL SYSTEMS MAGAZINE 17

Tariq Samad



the committee members.		
Rank and Technology	High-Impact Ratings	Low- or No-Impact Ratings
PID control	100%	0%
Model predictive control	78%	9%
System identification	61%	9%
Process data analytics	61%	17%
Soft sensing	52%	22%
Fault detection and identification	50%	18%
Decentralized and/or coordinated control	48%	30%
Intelligent control	35%	30%
Discrete-event systems	23%	32%
Nonlinear control	22%	35%
Adaptive control	17%	43%
Robust control	13%	43%
Hybrid dynamical systems	13%	43%

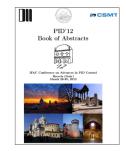
TABLE 1 A list of the survey results in order of industry impact as nerceived by

臣

▲圖 → ▲ 国 → ▲ 国 →

Problem statement and generic solution Specific Tuning Rules Robustness and Performance evaluation PID Tuning guidelines for Balanced Operation Concluding Remarks



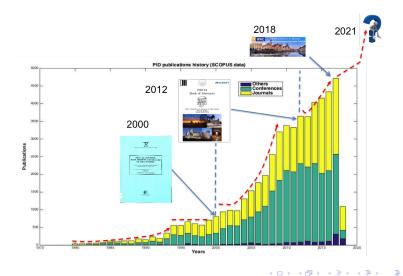


・ロト ・ 日 ・ ・ ヨ ・ ・ ヨ ・



æ

Problem statement and generic solution Specific Tuning Rules Robustness and Performance evaluation PID Tuning guidelines for Balanced Operation Concluding Remarks



The continued interest on PI(D) control is a fact

- From the practitioner's point of view
  - Reliability
  - Smooth control
  - Definition of loop specifications
  - Complement PID with help units
  - ...
- From the research point of view
  - Clear guidelines for the benefits of D term
  - Robustness should be transparently included
  - Incorporate tradeoffs and keep simplicity
  - Optimality or suboptimality?
  - ...

What has characterized the evolution of the PID controller and its design approaches is the formulation of tuning rules.

A new PID controller design scenario much more constrained

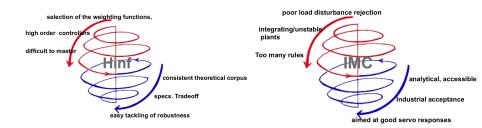
- Servo/Regulation Performance
- Moderate usage of control action
- Robustness
- Simple and clear formulations
- Include derivative term
- Measurement noise attenuation
- *tradeoff* (smoothness/robustness/reactivity)

## Global perspective

It is needed to rethink how to put play with these considerations, its interactions and formulate the overall design problem in the simplest possible way.



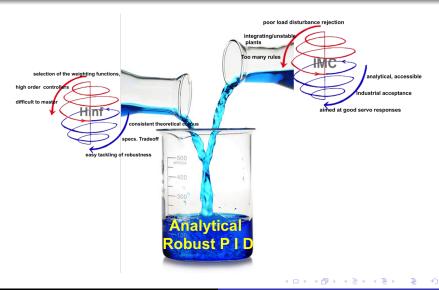
Among modern, advanced, control approaches, there are two well known and succeding approaches:



æ

(日) (四) (日) (日) (日)

Problem statement and generic solution Specific Tuning Rules Robustness and Performance evaluation PID Tuning guidelines for Balanced Operation Concluding Remarks



 $\bullet\,$  State the  ${\it H}_\infty$  problem for the weighted sensitivity function

# $\|WS\|_{\infty}$

- Appropriately parameterize the weight to represent the problems of interest
  - Servo / Regulation
  - Robustness / Performance
- Analytical solution in terms of the generalized IMC
- Interpret the solution in terms of the PID controller.

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

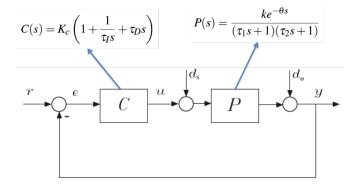
# 1 Motivation

- 2 Problem statement and generic solution
- 3 Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation
- 6 Concluding Remarks

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

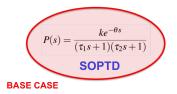
(D) (A) (A) (A)

## Let us consider the standard feedback setup



Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

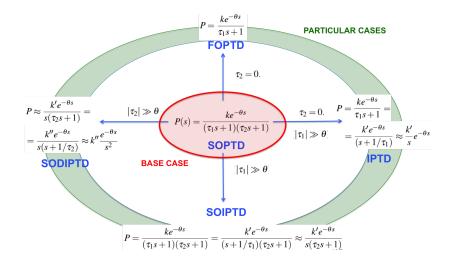
イロン イヨン イヨン イヨン



æ

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

イロン イヨン イヨン イヨン



æ

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

For design, we rely on the well-known Weighted Sensitivity problem

 $\min_{C\in\mathcal{C}}\|WS\|_{\infty}$ 

The following structure for the weight is adopted:

$$W = \left(\frac{(\lambda s + 1)}{s}\right) \left(\frac{(\gamma_1 s + 1)(\gamma_2 s + 1)}{(\tau_1 s + 1)(\tau_2 s + 1)}\right)$$

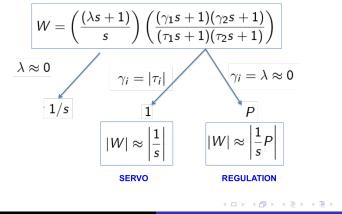
where  $\lambda > 0, \gamma_i \in [\lambda, |\tau_i|], i = 1, 2$ . An even more generic weight was analyzed in (Alcantara et al. 2011)<sup>†</sup>

<sup>†</sup>S. Alcántara, W. Zhang, C. Pedret, R. Vilanova, and S. Skogestad, *IMC-like* analytical  $H_{\infty}$  design with *S/SP* mixed sensitivity consideration: Utility in PID tuning guidance, Journal of Process Control, 2011.

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

18 / 73

The rationale behind the  $\lambda$  and  $\gamma$  parameters can be explained, quite heuristically, as follows. Remember  $\lambda > 0, \gamma_i \in [\lambda, |\tau_i|]$  and start by considering  $\lambda \approx 0$ , then:



Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

- Intermediate values for  $\gamma_1$  and  $\gamma_2$  will produce a balance between the purely servo and regulation situations.
- If we increase the value of  $\lambda$  (we assumed  $\lambda \approx 0$ ), the weight will progressively slow down the resulting closed-loop.
- Once  $\gamma_1, \gamma_2$  have been fixed,  $\lambda$  can be used to reach a balance between robustness and performance.

## weight selection and tradeoff issues

The selected weight allows us to deal with both tradeoffs

- robustness/performance (via  $\lambda$ )
- servo/regulation issues (via  $\gamma_1, \gamma_2$ ).

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

The solution of the Weighted Sensitivity problem goes as:

- Parameterize K in the IMC form  $K = Q(1 PQ)^{-1}$
- Rewrite the problem in terms of Q:  $\|W(1-PQ)\|_{\infty} = \|\mathcal{N}_o\|_{\infty}$
- The optimal  $\mathcal{N}_o$  is all-pass  $\mathcal{N}_o = \rho \frac{q(-s)}{q(s)}$
- Recover the optimal  $Q_o = P^{-1}(1 \mathcal{N}_o W^{-1})$
- Get the optimal sensitivity as  $S_o = 1 PQ_o = W\mathcal{N}_o$
- Recover the optimal feedback controller  $K_o = Q_o (1 PQ_o)^{-1}$

イロト イポト イヨト イヨト

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

In order to analytically solve the weighted sensitivity problem, we first approximate the time delay in the SOPTD model.

$$P = rac{Ke^{-Ls}}{( au_1s+1)( au_2+1)} pprox rac{k(- heta s+1)}{( au_1s+1)( au_2+1)}$$

By application of the maximum modulus principle, it turns out that

- the optimal weighted sensitivity is all-pass:  $WS^o = \rho$ .
- $\rho$  is given by

$$\rho = |W|_{s=\frac{1}{\theta}} = \frac{(\lambda + \theta)(\gamma_1 + \theta)(\gamma_2 + \theta)}{(\tau_1 + \theta)(\tau_2 + \theta)}$$

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

From the expression for the optimal sensitivity we can get the optimal controller as a PID:

$$C^{o} = P^{-1}(\rho^{-1}W - 1) = \frac{\zeta_{2}s^{2} + \zeta_{1}s + 1}{\rho ks} = \frac{\zeta_{1}}{\rho k} \left(1 + \frac{1}{\zeta_{1}s} + \frac{\zeta_{2}}{\zeta_{1}}s\right)$$

with

$$\zeta_{1} = \frac{\theta((\tau_{1}+\tau_{2}-\lambda)(\gamma_{1}+\gamma_{2})+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(\gamma_{1}+\gamma_{2}+\lambda+\theta)-\gamma_{1}\gamma_{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)}$$

$$\zeta_{2} = \frac{\tau_{1}\tau_{2}((\lambda+\theta)(\gamma_{1}+\gamma_{2})+\gamma_{1}\gamma_{2}+\lambda\theta+\theta^{2})-\gamma_{1}\gamma_{2}\lambda(\theta+\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)}$$

## ANALYTIC H<sub>inf</sub> PID TUNING FOR SOPTD

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

It is possible however to formulate the analysis that follows with a simplification regarding the  $\gamma's.$ 

- What is strictly necessary in the weight is to have a zero for every plant pole.
- If we have two different  $\gamma's$  we will have more freedom for the design, but this is not strictly necessary.
- In order to simplify, we can set  $\gamma_1 = \gamma_2 = \gamma$ . Then with  $\lambda > 0$  and  $\gamma \in [\lambda, \tau]$ , where we have defined

$$\tau \doteq \max(|\tau_1|, |\tau_2|) = |\tau_1|.$$

Servo/Regulation and Robustness tradeoff Unifying PID tuning rules

・ロト ・ 日 ・ ・ ヨ ・ ・ ヨ ・ ・

æ

24 / 73

$$\begin{split} & \underset{C \in \mathcal{C}}{\min} \|WS\|_{\infty} \qquad \qquad \lambda, \gamma_{1}, \gamma_{2}. \\ \\ \zeta_{1} &= \frac{\theta((\tau_{1}+\tau_{2}-\lambda)(\gamma_{1}+\gamma_{2})+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(\gamma_{1}+\gamma_{2}+\lambda+\theta)-\gamma_{1}\gamma_{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)} \\ & \zeta_{2} &= \frac{\tau_{1}\tau_{2}((\lambda+\theta)(\gamma_{1}+\gamma_{2})+\gamma_{1}\gamma_{2}+\lambda\theta+\theta^{2})-\gamma_{1}\gamma_{2}\lambda(\theta+\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)} \\ \\ \hline K_{c} &= \frac{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{k(\lambda+\theta)(\gamma+\theta)^{2}} \\ \tau_{1} &= \frac{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)} \\ \hline T_{D} &= \frac{\tau_{1}\tau_{2}(2\gamma(\lambda+\theta)+\gamma^{2}+\lambda\theta+\theta^{2})-\gamma^{2}\lambda(\theta+\tau_{1}+\tau_{2})}{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}} \\ \hline \end{array}$$

# Motivation

2 Problem statement and generic solution

# 3 Specific Tuning Rules

- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation

# 6 Concluding Remarks

The previous, messy, expressions constitute the tuning assignment for the most general case. There are some special cases of which deserve specific attention.

- First Order Plus Time Delay (FOPTD)
- Integrating Plus Time Delay (IPTD)
- Second Order Plus Time Delay (SOPTD)
- Second Order Integrating Plus Time Delay (SOIPTD)
- Second Order Double Integrating Plus Time Delay (SODITD)

Will present the corresponding tuning assignments just to show how they derive from the general case.

(D) (A) (A) (A)

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

For a First Order Plus Time Delay (FOPTD) we get a PI controller

$$P(s) = \frac{ke^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)}$$

$$V = \left(\frac{(\lambda s + 1)}{s}\right) \left(\frac{(\gamma_1 s + 1)(\gamma_2 s + 1)}{(\tau_1 s + 1)(\tau_2 s + 1)}\right)$$

$$V = \gamma_1, \gamma_2 = 0$$

æ

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

・ロト ・ 同ト ・ ヨト ・ ヨト

# For a Integrating Plus Time Delay (IPTD) we get a PI controller

$$P(s) = \frac{ke^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)} \qquad \begin{array}{c} \tau_2 = 0, \quad k' = \frac{k}{\tau_1} \\ \hline \tau_1 \gg \theta \end{array} \qquad P = \frac{k'e^{-\theta s}}{(s + 1/\tau_1)} \approx \frac{k'}{s}e^{-\theta s}$$

$$W = \left(\frac{(\lambda s + 1)}{s}\right) \left(\frac{(\gamma_1 s + 1)(\gamma_2 s + 1)}{(\tau_1 s + 1)(\tau_2 s + 1)}\right) \qquad \gamma = \gamma_1, \gamma_2 = 0$$

$$K_c = \frac{\gamma + \lambda + \theta}{k'(\lambda + \theta)(\gamma + \theta)} \quad \tau_l = \gamma + \lambda + \theta$$

$$\lambda > 0, \gamma \in [\lambda, \infty)$$

æ

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

(D) (A) (A) (A)

For a Second Order Plus Time Delay (SOPTD), this is the original base problem, but we get simple expressions with:

$$\gamma_1 = \gamma_2 = \gamma \quad \tau \doteq \max\{|\tau_1|, |\tau_2|\} = |\tau_1|$$

$$\begin{split} \mathcal{K}_{c} &= \frac{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{k(\lambda+\theta)(\gamma+\theta)^{2}}\\ \tau_{I} &= \frac{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})}{(\tau_{1}+\theta)(\tau_{2}+\theta)}\\ \tau_{D} &= \frac{\tau_{1}\tau_{2}(2\gamma(\lambda+\theta)+\gamma^{2}+\lambda\theta+\theta^{2})-\gamma^{2}\lambda(\theta+\tau_{1}+\tau_{2})}{\theta(2\gamma(\tau_{1}+\tau_{2}-\lambda)+\lambda(\tau_{1}+\tau_{2}))+\tau_{1}\tau_{2}(2\gamma+\lambda+\theta)-\gamma^{2}(\lambda+\theta)+\theta^{2}(\tau_{1}+\tau_{2})} \end{split}$$

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Integrating Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

イロン イヨン イヨン イヨン

# For a Second Order Integrating Plus Time Delay (SOIPTD) we get a PID controller

$$P(s) = \frac{ke^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)} \xrightarrow{||\tau_1| \gg \theta} P = \frac{k'e^{-\theta s}}{(s + 1/\tau_1)(\tau_2 s + 1)} \approx \frac{k'e^{-\theta s}}{s(\tau_2 s + 1)}$$

$$W = \left(\frac{(\lambda s + 1)}{s}\right) \left(\frac{(\gamma_1 s + 1)(\gamma_2 s + 1)}{(\tau_1 s + 1)(\tau_2 s + 1)}\right) \xrightarrow{\gamma = \gamma_1 = \gamma_2}$$

$$K_c = \frac{(\tau_2 + \theta)(\theta + 2\gamma + \lambda)}{k'(\lambda + \theta)(\gamma + \theta)^2} \quad \lambda > 0, \gamma \in [\lambda, \infty)$$

$$\tau_D = \frac{\tau_2((\gamma + \theta)(\theta + 2\gamma + \lambda)}{(\tau_2 + \theta)(\theta + 2\gamma + \lambda)}$$

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

For a Second Order Double Integrating Plus Time Delay (SODITD) we get a PID controller

 $P(s) = \frac{ke^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)} \xrightarrow{||\tau_1| \gg \theta} P = \frac{k'e^{-\theta s}}{(s + 1/\tau_1)(\tau_2 s + 1)} \approx \frac{k'e^{-\theta s}}{s(\tau_2 s + 1)}$   $P \approx \frac{k'e^{-\theta s}}{s(\tau_2 s + 1)} = \frac{|\tau_2| \gg \theta}{k'' = \frac{k'}{\tau_2}}$   $= \frac{k''e^{-\theta s}}{s(s + 1/\tau_2)} \approx k'' \frac{e^{-\theta s}}{s^2}$  $W = \left(\frac{(\lambda s+1)}{s}\right) \left(\frac{(\gamma s+1)(\gamma s+1)}{(\tau s+1)(\tau s+1)}\right) \qquad \qquad \gamma = \gamma = \gamma_2$  $\begin{array}{lll} K_c & = & \frac{\theta + 2\gamma + \lambda}{k''(\lambda + \theta)(\gamma + \theta)^2} \\ \tau_I & = & \theta + 2\gamma + \lambda \\ \tau_D & = & \frac{(\gamma + \theta)^2 + \lambda(2\gamma + \theta)}{\gamma + 2\gamma + \lambda} \end{array} \\ \end{array}$ ◆□▶ ◆□▶ ◆三▶ ◆三▶ ○○ ○○○

R. Vilanova, IFAC2020 PID Workshop

First Order Plus Time Delay (FOPTD) Integrating Plus Time Delay (IPTD) Second Order Plus Time Delay (SOPTD) Second Order Integrating Plus Time Delay (SOIPTD) Second Order Double Integrating Plus Time Delay (SODITD)

So far, we got a whole set of tuning rules for different process dynamics

- All of them originate from the original weighted sensitivity problem
- The structure of the controller arises from the structure of the problem solution
- $\bullet$  All of them are expressed in terms of the  $\gamma\lambda$  parameters
- What is left ?
  - Provide selection for  $\gamma\lambda$
  - Generate automatic tuning rules

Robustness and comparable designs Performance (Servo/Regulation) evaluation

# Motivation

- Problem statement and generic solution
- 3 Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation
- 6 Concluding Remarks

Robustness and comparable designs Performance (Servo/Regulation) evaluation

Let us consider the particular example of applying a pure servo and pure regulation design to the process

$$P(s) = \frac{5e^{-s}}{(20s+1)}$$

• Pure servo design:  $\lambda = \theta (= 1), \ \gamma = \tau (= 20)$ 

$$Kc = 2.0$$
  $T_i = 20.0$   $M_S \approx 1.6$ 

• Pure regulation design:  $\lambda = \theta (= 1), \ \gamma = \lambda (= 1)$ 

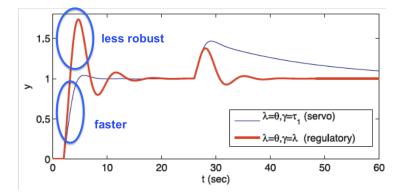
$$Kc = 2.95$$
  $T_i = 2.8$   $M_S \approx 3$ 

Regulatory design: faster (large gains) but less robust (higher  $M_S$ ).

Robustness and comparable designs Performance (Servo/Regulation) evaluation

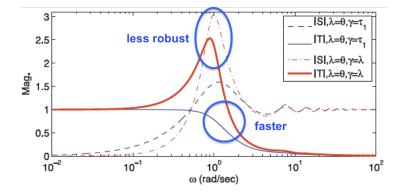
イロト イヨト イヨト イヨト

## Time domain effects of faster but less robust design



Robustness and comparable designs Performance (Servo/Regulation) evaluation

### Frequency domain effects of faster but less robust design



臣

Robustness and comparable designs Performance (Servo/Regulation) evaluation

The previous situation is not particular of the example but general <sup>†</sup>:

Regulatory control is based on shifting the slow poles of the plant whereas servo control aims at cancelling them (as long as possible) to flatten out the frequency response.

#### servos vs. regulation

Therefore, the comparison between the regulator and servo designs is left with a faster and less robust, vs a slower and more robust alternative.

† R. H. Middleton and S. F. Graebe, Slow stable open-loop poles: to cancel or not to cancel, Automatica, vol. 35, no. 5, pp, 877-886, 1999, 3

Robustness and comparable designs Performance (Servo/Regulation) evaluation

In (Middleton, 1999)<sup> $\dagger$ </sup> the notion of Extreme Frequency Equivalence is introduced in order to make two designs comparable:

#### Extreme Frequency Equivalence (EFE)

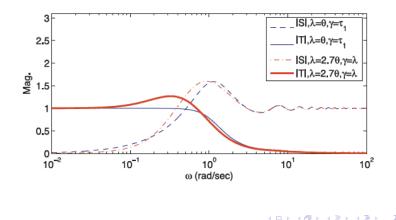
extreme frequency equivalent complementary sensitivities posses similar initial rise time and the same sensitivity to high-frequency noise and modelling errors.

In the previous example we increase the value of  $\lambda$  in the regulator mode until making the servo and regulatory designs comparable in the EFE sense.

† R. H. Middleton and S. F. Graebe, *Slow stable open-loop poles: to cancel or not to cancel*, Automatica, vol. 35, no. 5, pp. 877-886, 1999.

Robustness and comparable designs Performance (Servo/Regulation) evaluation

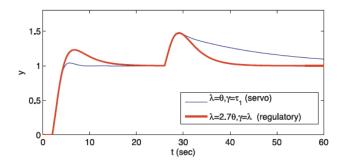
Now we have similar values for the sensitivity peaks (robustness and sensitivity) as well as bandwidth



Robustness and comparable designs Performance (Servo/Regulation) evaluation

Image: A match the second s

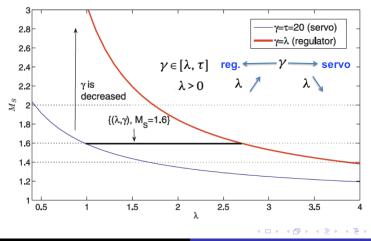
The effect of the EFE can also be appreciated in the time responses.



э

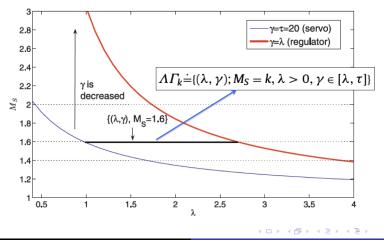
Robustness and comparable designs Performance (Servo/Regulation) evaluation

As we reduce  $\gamma$  to improve regulatory control, then  $\lambda$  has to increase to compensate for robustness (in the EFE sense)



Robustness and comparable designs Performance (Servo/Regulation) evaluation

For a specified robustness level we can define the following design space for  $\gamma\lambda$ 



Robustness and comparable designs Performance (Servo/Regulation) evaluation

In order to face the problem of balancing the servo and regulatory performance (select  $\gamma$ ), we consider the minimization of two alternative performance indices:

$$egin{array}{rcl} J_{\max} &=& \max(\Delta_s,\Delta_r) \ J_{\mathrm{avg}} &=& 0.5(\Delta_s+\Delta_r) \end{array}$$

where

$$\Delta_s = \frac{\mathsf{IAE}_s}{\mathsf{IAE}_s^o} \ \Delta_r = \frac{\mathsf{IAE}_r}{\mathsf{IAE}_r^o}$$

and

$$\mathsf{IAE} = \int_0^\infty |r(t) - y(t)| dt = \int_0^\infty |e(t)| dt$$

The optimal IAE<sup>o</sup><sub>s</sub> and IAE<sup>o</sup><sub>r</sub> are calculated over  $\Lambda\Gamma_k$ .

Robustness and comparable designs Performance (Servo/Regulation) evaluation

Regarding the two performance indices

- $J_{avg} = 0.5(\Delta_s + \Delta_r)$  is used in [1] to evaluate the SIMC-PI method, and it weighs the importance of servo and regulatory performance about equally
- $J_{\max} = \max(\Delta_s, \Delta_r)$  already considered in [2], it adheres to the common strategy in multiobjective optimization of minimizing the worst case performance

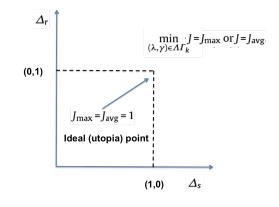
Importantly, both are sound performance measures, independent of the process gain, the disturbance and set-point magnitudes, and of the units used for time

[1] C. Grimholt and S. Skogestad, Optimal PI Control and Verifcation of the SIMC Tuning Rule, in Proc. of the IFAC Conf. on Advances in PID Control PID'12, 2012.

[2] S. Alcántara, R. Vilanova, C. Pedret, and S. Skogestad, A look into robustness/performance and servo/regulation issues in PI tuning, in Proc. of DID Control DID'10 2010

Robustness and comparable designs Performance (Servo/Regulation) evaluation

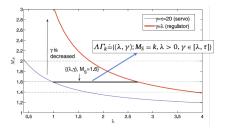
Then, for each robustness level  $(M_S = k)$ , we will consider the following optimization problem



Robustness and comparable designs Performance (Servo/Regulation) evaluation

Regarding the definition of the performance degradation and performance indices the following has to be noticed.

- As the design gets more robust, λ increases and the interval for γ ∈ [λ τ], gets smaller
- In high robustness designs, the servo/regulator trade-off tends to disappear
- $J_{\rm avg} \approx 1$  and  $J_{\rm max} \approx 1$  are obtained.



This is misleading from a robustness/performance point of view, since high robustness should imply low performance, i.e.  $J \gg 1$ 

Robustness and comparable designs Performance (Servo/Regulation) evaluation

(D) (A) (A) (A)

In order to study the trade-off between robustness and performance in absolute terms, it will be better to consider the

globally optimal IAE values over the set  $\bigcup_k \Lambda \Gamma_k \forall k$ .

The performance degradation is redefined as follows:

$$\Delta_s^* = \frac{\mathsf{IAE}_s}{\mathsf{IAE}_s^{go}} \ , \ \Delta_r^* = \frac{\mathsf{IAE}_r}{\mathsf{IAE}_r^{go}}$$

•  $IAE_s^{go}$  and  $IAE_r^{go}$  are computed over  $\bigcup_k \Lambda \Gamma_k$ 

•  $IAE_s$  and  $IAE_r$  are computed over  $\Lambda\Gamma_k$ 

Accordingly  $J^*_{\mathsf{avg}} = 0.5(\Delta^*_s + \Delta^*_r)$  and  $J^*_{\mathsf{max}} = \mathsf{max}(\Delta^*_s, \Delta^*_r)$ 

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

## Motivation

- Problem statement and generic solution
- 3 Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation

### 6 Concluding Remarks

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

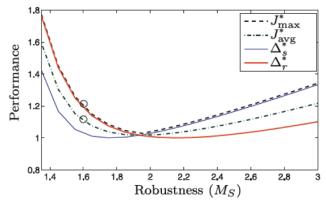
イロト イポト イヨト イヨト

The analysis conducted so far has lead us to generic  $\lambda\gamma$  expressions for a PI and a PID.

Now we will proceed to analyze the selection of the tuning parameters  $\lambda, \gamma$  and to provide tuning guidelines to achieve a *balanced* closed-loop.

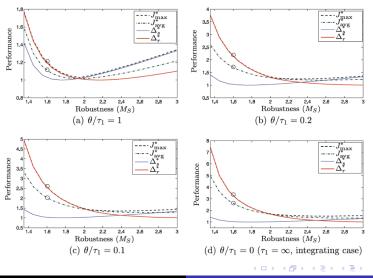
- **(**) Analyze the evolution of the performance indexes  $J_{avg}^*$  and  $J_{max}^*$
- Consider the robustness/performance trade-off to see if we can specify a constant target robustness level.
- Study how to select the  $\lambda$  and  $\gamma$  parameters by solving the optimization problem for  $k = M_S^t$ .
- Suggest specific choice to generate an automatic tuning.

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



- Interested in the negative or zero derivative zone
- If  $M_s > 2$  both Perf. and Rob can be improved simultaneously
- Servo/regulator tradeoff important is the blue and red plots are separated.
- $M_s^t \approx 1.6$  provides a good choice for the tradeoff

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



R. Vilanova, IFAC2020 PID Workshop Unified perspective to PID Tuning

æ

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

$ heta/ au_1 < 1$ $\lambda = 1.25 heta$	$ heta/ au \ge \lambda pprox$		$\lambda = 2.5 \theta$		
$J = J_{\max}$			$J = J_{\rm avg}$		
$ heta/ au_1$	$\lambda/ heta$	$\gamma/\lambda$	$ heta/ au_1$	$\lambda/ heta$	$\gamma/\lambda$
1	1	1	1	1	1
0.2	1.1887	3.1125	0.2	2	1
0.1	1.2406	4.5947	0.1	2.4	1
0.05	1.2718	6.1329	0.05	2.693	1.0026
0.02	1.2840	7.9437	0.02	2.9	1
$0 \ (\tau_1 = \infty)$	1.3085	9.1708	$0 \ (\tau_1 = \infty)$	3.0213	1.026
					[

$$\gamma = \lambda$$

イロン イヨン イヨン イヨン

3

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

イロン イヨン イヨン イヨン

$$P = \frac{ke^{-\theta s}}{\tau_{1}s+1} \begin{cases} K_{c} = \frac{\tau_{1}(\gamma + \lambda + \theta) - \lambda\gamma}{k(\lambda + \theta)(\gamma + \theta)} \\ \tau_{I} = \frac{\tau_{1}(\gamma + \lambda + \theta) - \lambda\gamma}{\tau_{1} + \theta \text{ FOPTD}} \end{cases} \qquad K_{c} = \frac{\gamma + \lambda + \theta}{k'(\lambda + \theta)(\gamma + \theta)} \\ \tau_{I} = \gamma + \lambda + \theta \end{cases} P = \frac{k'}{s}e^{-\theta s}$$

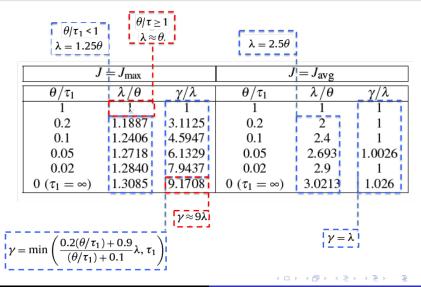
$$IPTD$$

$$\downarrow \lambda = 2.5\theta \qquad \gamma = \lambda$$

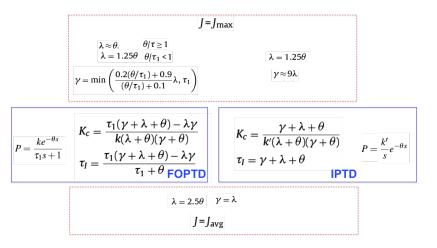
$$J = J_{avg}$$

э.

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



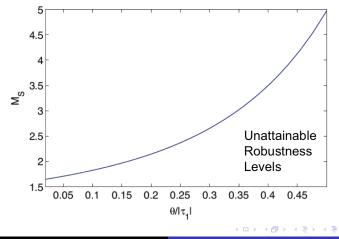
Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



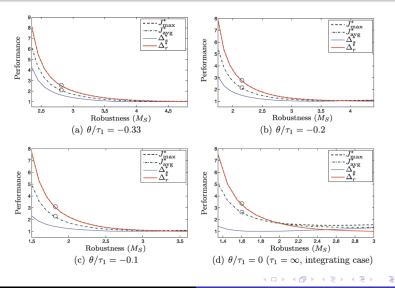
<ロ> (四) (四) (三) (三) (三)

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

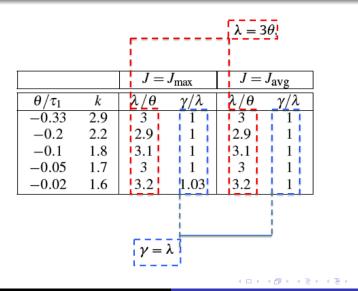
For unstable plants  $M_S$  gets very large values. One should limit the use of the tuning to plants with  $\theta/|\tau_1| < 0.5$  approximately.



Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



3

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

イロン イヨン イヨン イヨン

$$P = \frac{ke^{-\theta s}}{\tau_1 s + 1}$$

$$K_c = \frac{\tau_1(\gamma + \lambda + \theta) - \lambda\gamma}{k(\lambda + \theta)(\gamma + \theta)}$$

$$\tau_I = \frac{\tau_1(\gamma + \lambda + \theta) - \lambda\gamma}{\tau_1 + \theta}$$

$$V = \lambda$$

$$k_c = \frac{7\tau_1 - 9\theta}{k16\theta}$$

$$\tau_I = \frac{7\tau_1 - 9\theta}{(\tau_1/\theta) + 1}$$

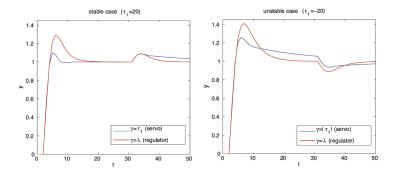
J=Javg & J=Jmax

3

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

・ロト ・ 同ト ・ ヨト ・ ヨト

In this case the analysis conducted suggests regulatory design  $(\lambda = \gamma)$  and  $\gamma \approx 3\theta$  for both  $J^*_{avg}$  and  $J^*_{max}$ 



60 / 73

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

・ロト ・ 同ト ・ ヨト ・ ヨト

For the second order case we considered the simplification

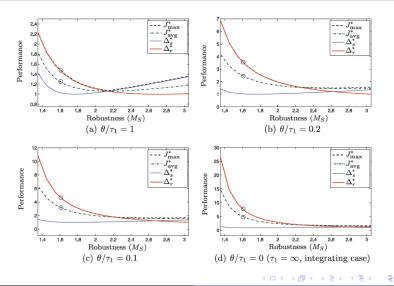
$$\gamma_1 = \gamma_2 = \gamma \quad \tau \doteq \max\{|\tau_1|, |\tau_2|\} = |\tau_1|$$

This is well motivated for the double pole case

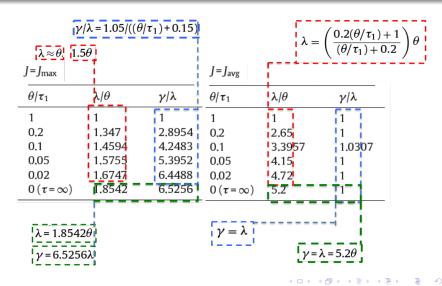
$$P = \frac{ke^{-\theta s}}{\left(\tau_1 s + 1\right)^2}$$

- $\bullet\,$  Analisys gets simple as it only depends on  $\theta/\tau$
- Results mainly depend on the dominant time constant.
- The resulting tuning guidelines can also be applied to the general SOPTD model for which  $\tau_1 \neq \tau_2$

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



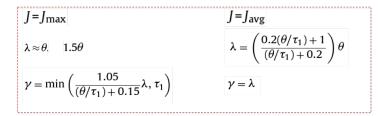
Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes



Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

・ロト ・聞 ト ・ ヨト ・ ヨトー

$$P = \frac{ke^{-\theta s}}{(\tau_1 s + 1)^2} \qquad K_c = \frac{2\theta(\gamma(2\tau_1 - \lambda) + \lambda\tau_1) + \tau_1^2(2\gamma + \lambda + \theta) - \gamma^2(\lambda + \theta) + 2\theta^2\tau_1}{k(\lambda + \theta)(\gamma + \theta)^2}$$
$$\tau_I = \frac{2\theta(\gamma(2\tau_1 - \lambda) + \lambda\tau_1) + \tau_1^2(2\gamma + \lambda + \theta) - \gamma^2(\lambda + \theta) + 2\theta^2\tau_1}{(\tau_1 + \theta)^2}$$
$$\tau_D = \frac{\tau_1^2(2\gamma(\lambda + \theta) + \gamma^2 + \lambda\theta + \theta^2) - \gamma^2\lambda(\theta + 2\tau_1)}{2\theta(\gamma(2\tau_1 - \lambda) + \lambda\tau_1) + \tau_1^2(2\gamma + \lambda + \theta) - \gamma^2(\lambda + \theta) + 2\theta^2\tau_1}$$

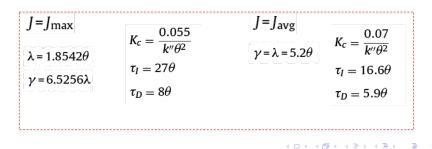


Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

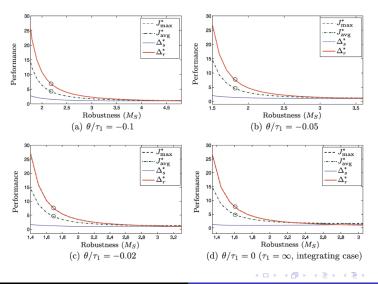
$$P \approx \frac{k'e^{-\theta s}}{s(\tau_2 s + 1)} = \frac{k''e^{-\theta s}}{s(s + 1/\tau_2)} \approx k''\frac{e^{-\theta s}}{s^2}$$

$$K_{c} = \frac{\theta + 2\gamma + \lambda}{k''(\lambda + \theta)(\gamma + \theta)^{2}}$$
$$\tau_{I} = \theta + 2\gamma + \lambda$$
$$\tau_{D} = \frac{(\gamma + \theta)^{2} + \lambda(2\gamma + \theta)}{\theta + 2\gamma + \lambda}$$

SODIPTD



Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

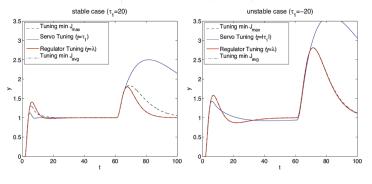


æ

Stable and Integrating First Order Processes Unstable First Order Processes Stable and Integrating Second Order Processes Unstable Second Order Processes

In this case the analysis conducted suggests regulatory design ( $\lambda = \gamma$ ) and  $\gamma \approx 5.2\theta$  for both  $J^*_{avg}$  and  $J^*_{max}$ 

$$P = 50e^{-s}/(\tau_1 s + 1)^2$$
  $M_s = 1.8.$ 



э

## Motivation

- Problem statement and generic solution
- 3 Specific Tuning Rules
- 4 Robustness and Performance evaluation
- 5 PID Tuning guidelines for Balanced Operation
- 6 Concluding Remarks

- It is possible to encompass PI/D design within a modern control theory viewpoint
- The problem is solved in the two parameter space  $\lambda \gamma$  instead of the original  $K_c$ ,  $T_i$ ,  $T_d$  space
  - we may not get the truly optimal
  - better to analyze the robustness/performance servo/regulation tradeoff
- The treatment is unifying as the same approach and root solution applies for a ser of process dynamics
- for particular selections, tuning result into already know ones
  - $\gamma= au_1$  we get the IMC designs
  - other particular cases for concrete published tunings

(D) (A) (A) (A)

Regarding the servo/regulation performance, two indexes have been considered:  $J^*_{\rm avg}$  and  $J^*_{\rm max}$ 

- For stable dynamics  $J^*_{avg}$  favours regulatory operation
- For stable dynamics  $J^*_{\max}$  results in a more balanced servo/regulator trade-off
  - sometimes yielding a sluggish closed-loop
  - designs less sensitive to modelling errors
- For unstable dynamics the option is to go for regulatory operation

#### Confirms usual practice

Regulatory control is the preferred option in general terms, justifying the common practice of considering only input disturbances,

(D) (A) (A) (A)

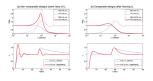
There is still much work to be done:

- For FO dynamics PI is suggested,... but would PID provide other benefits?
- What about oscillating dynamics
- Explore different ways of wheigthing servo/regulation/robustness
- Implications of other (more practical) formulations for the PID



# **PID TUNING**

A Modern Approach via the Weighted Sensitivity Problem



Salvador Alcántara Cano Ramon Vilanova Arbós Carles Pedret i Ferré

CRC Press

イロン イヨン イヨン

R. Vilanova, IFAC2020 PID Workshop

Unified perspective to PID Tuning

臣

PID tuning tackling design tradeoffs from an unified perspective

### Ramon Vilanova Dept. Telecomunications and Systems Engineering Universitat Autónoma de Barcelona, Barcelona

Workshop "Advanced Topics in PID Control System Design, Automatic Tuning and Applications" 21st IFAC World Congress, Germany July 12, 2020